

Recovering values from water industry by-products

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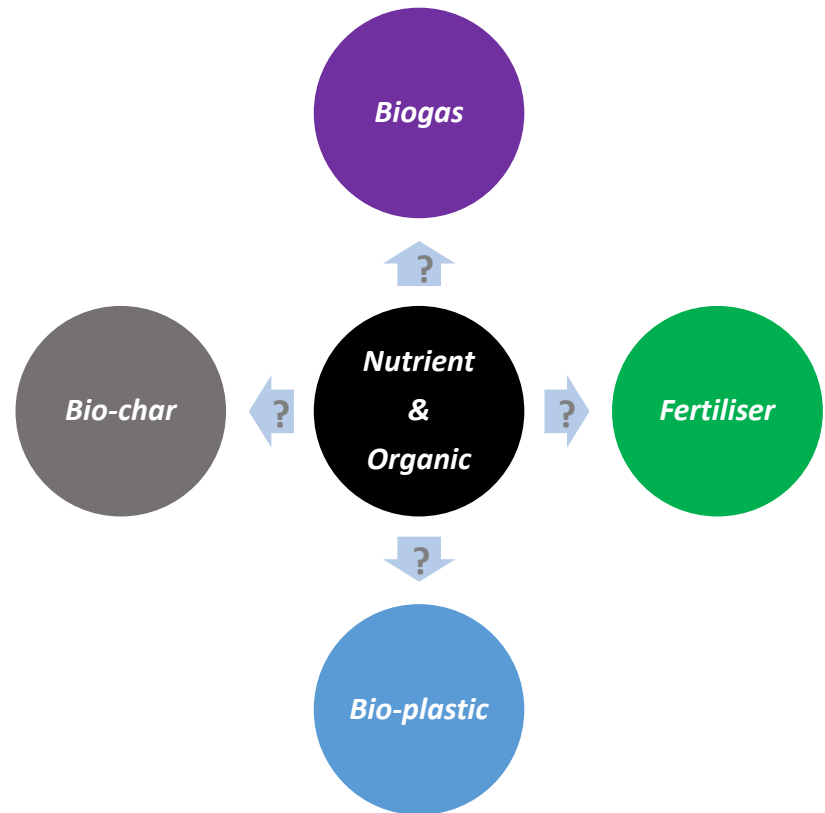
Project Brief

Research Question:

- *How much valuables flow in?*
- *Where and How they get removed or captured?*
- *Where and how to recover them?*
- *Is the mass loading of the recoverable valuables big enough to create **impacts** on **treatment performance, sustainability and economics**?*

Approach:

Mass and Energy Balance



Mass and Energy Balance Investigation

- **Actual Wastewater Treatment Work**

Howdon, Hendon, Allers and Laighpark

- **Composite Sample of Every Stream**

- *Wastewater : Inlet, Settled, Final Effluent, Return Liquor, etc.*
- *Sludge: Primary, Secondary, Digested, etc.*

- **Parameters**

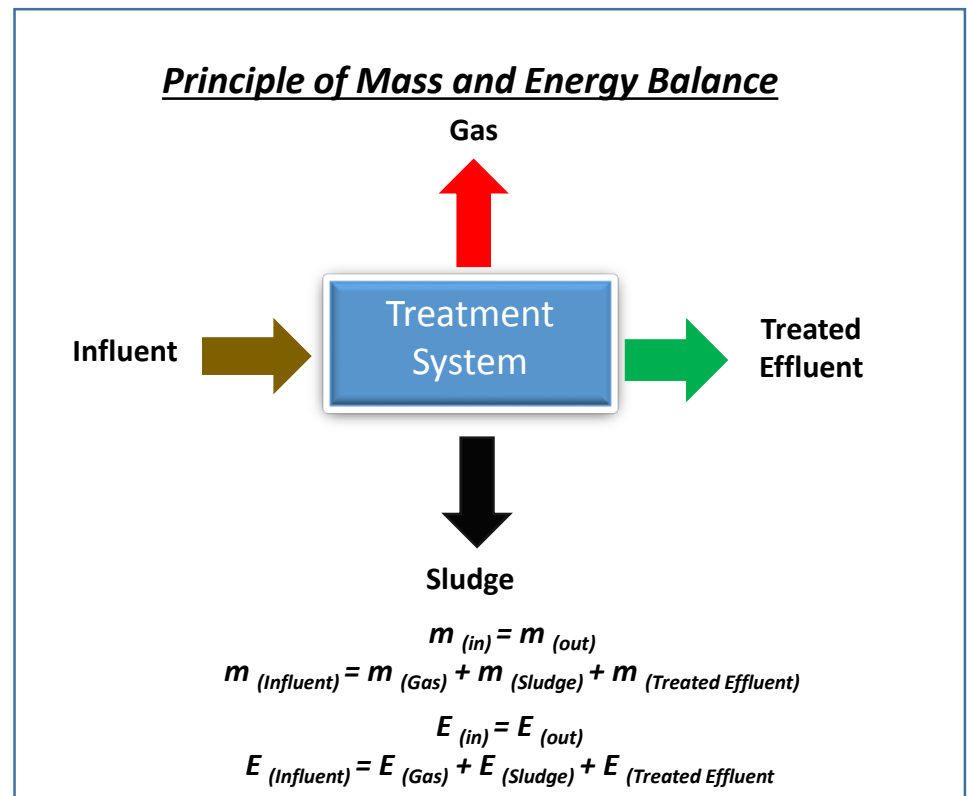
Wastewater

- *COD, sCOD, TOC, DOC*
- *AmmN, TKN, O-PO₄*
- *TS*
- *Energy*

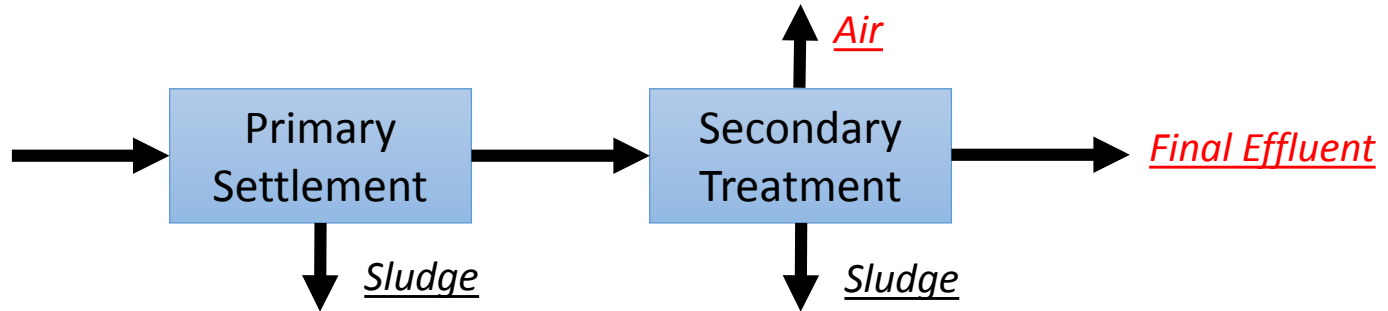
Sludge

- *TS, VS*
- *TOC, TN, TP*
- *Fibre – Hemicellulose, Cellulose and Lignin*
- *Energy*

$$\text{Mass} = \text{Flow} \times \text{Concentration}$$

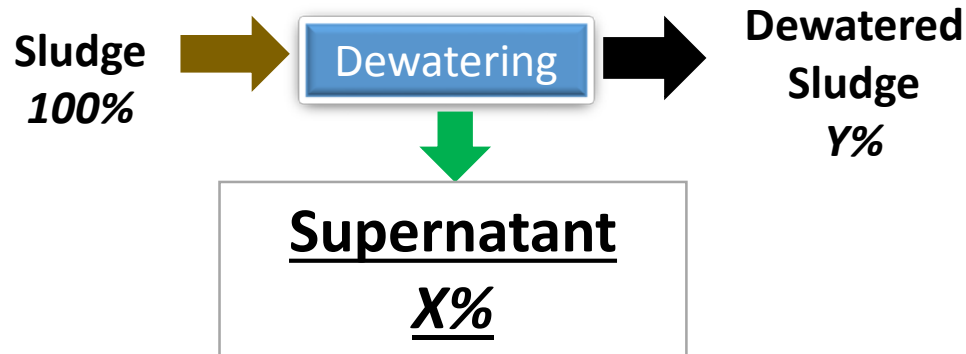


Nutrient in Wastewater Treatment



	N	P
Form of Existence	NH_4^+ , Organic N	PO_4^{3-} , Organic P
Treatment	<p>Biological (Secondary Treatment), Nitrification and Denitrification</p> <p>$\text{NH}_4^+ \rightarrow \text{NO}_3^-$ (In Effluent) $\rightarrow \text{N}_2$ (In Air)</p> <p>$\text{NH}_4^+ \rightarrow$ <i>Organic N (In Secondary Sludge)</i> *</p>	<p>Chemical (Primary Treatment)</p> <p>$\text{PO}_4^{3-} \rightarrow \text{FePO}_4$ or AlPO_4 (In Primary Sludge)</p> <p>Biological (Secondary Treatment)</p> <p>$\text{PO}_4^{3-} \rightarrow$ <i>Organic P (In Secondary Sludge)</i> *</p>
Capturing Rate	20-30%	30-90%

Nutrient in the Supernatant



	X% N-NH ₄ in Supernatant	X% P-PO ₄ in Supernatant
Primary	3-5%	3-6%
Secondary	3-5%	5-10%
Stored Sludge	<u>15-20%</u>	<u>30-40%</u>
Digested Sludge	<u>50-80%</u>	<u>20-40%</u>
Total Recoverable from <u>Sludge</u>	60-90%	50-60%
Total Recoverable from <u>Wastewater</u>	12-30%	15-50%

Recirculate to head of the work!!

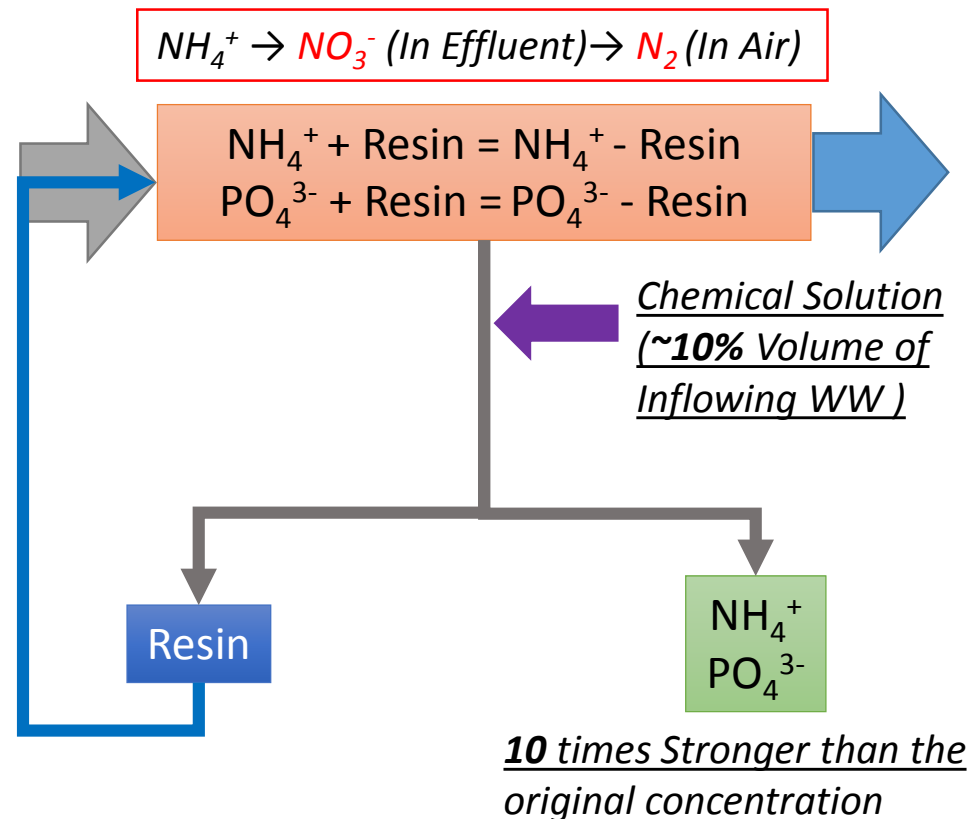
The nutrient loading to the WwTW is increased.

Recovering Nutrient Directly from Wastewater

Loading = Concentration x Flow

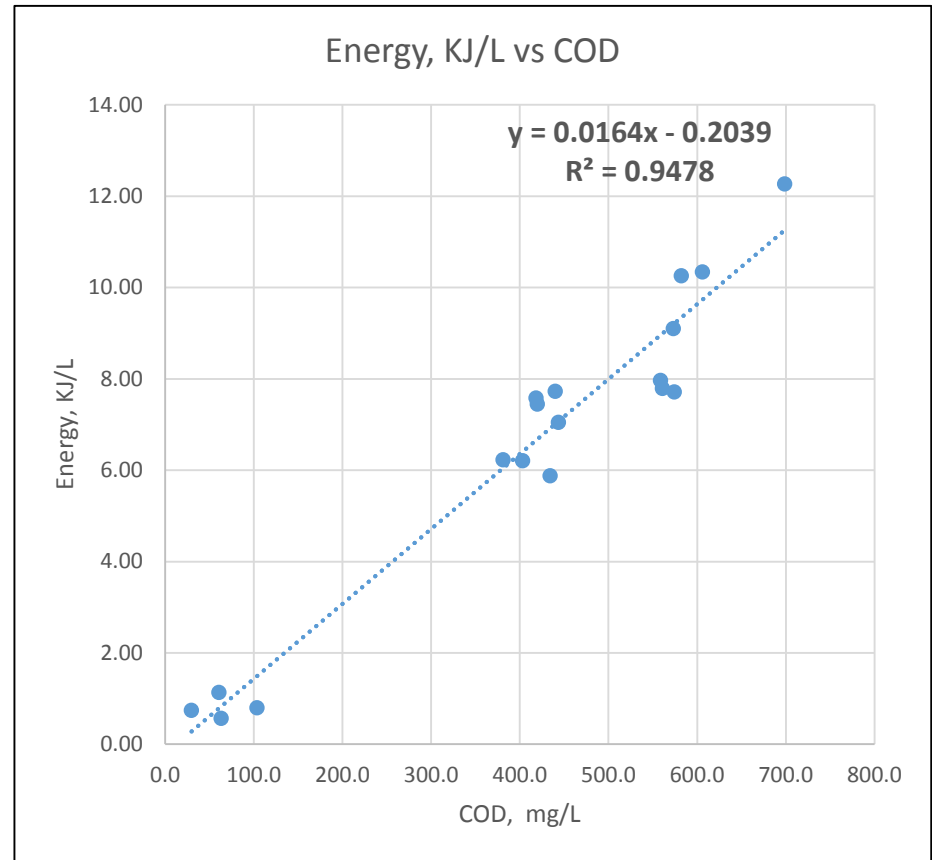
	Raw Wastewater	Return Liquor
Flow, m ³	270,000	8,500
AmmN, mg/L	30	211
AmmN, t	8.0	1.8
P-PO ₄ , mg/L	3	70
P-PO ₄ , t	0.8	0.6

- Though the nutrient concentration in the raw wastewater is low, considerable amount of nutrient is lost in **Air/Final Effluent**, especially the loss of Ammonium in nitrification and denitrification.

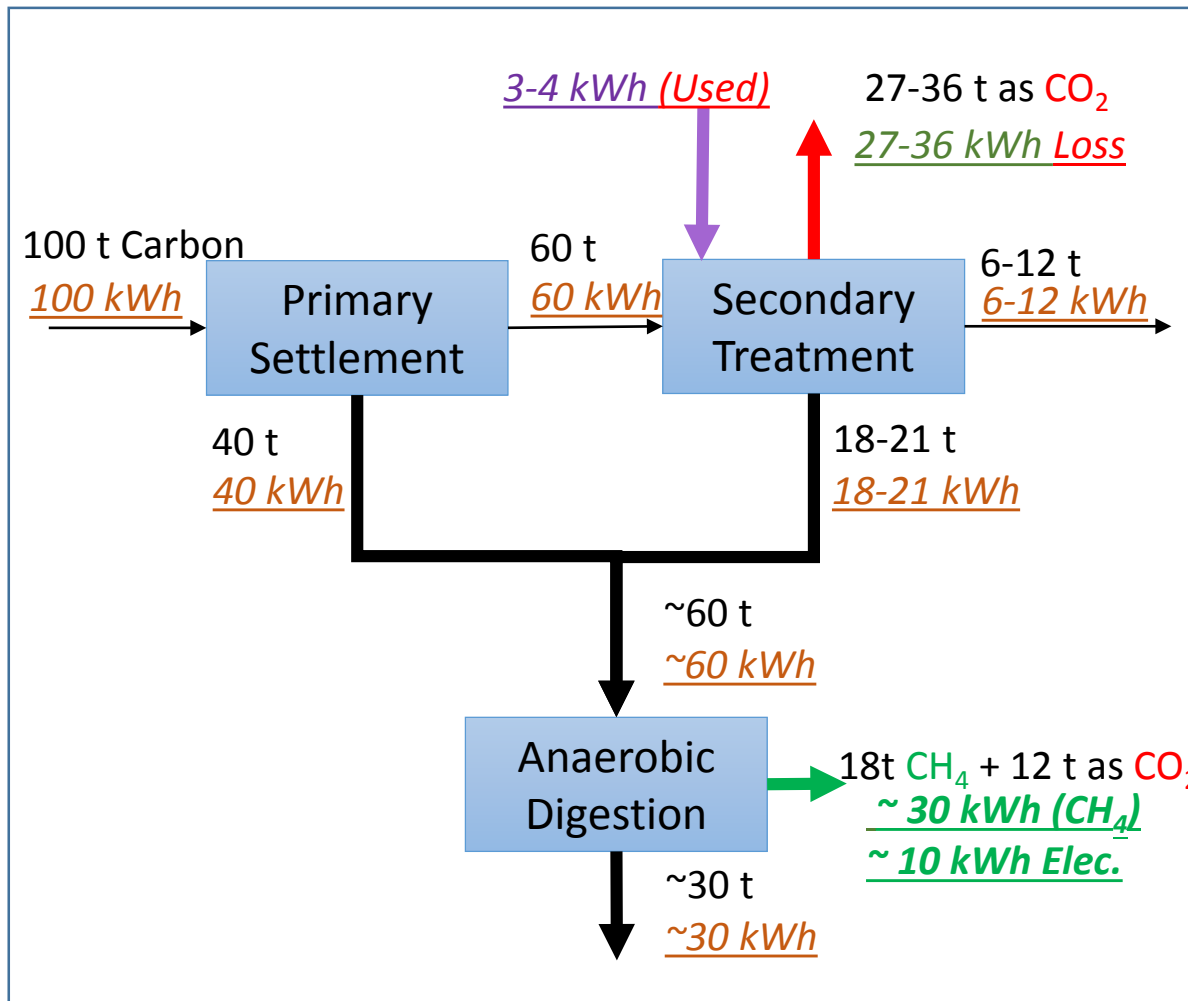


Carbon and Energy

- **0.25-1 kWh** electrical energy is used to treat 1 m³ of wastewater
- 1 gram of COD has about 16 KJ of **chemical** energy
- For a medium strength of wastewater with 500 mg/L COD, 1 m³ of wastewater has **2.22 kWh** of **chemical** energy
- If the conversion rate of chemical energy to electrical energy is **35%**, 1 m³ of wastewater has **0.77 kWh** of **electrical** energy
- Potentially, wastewater treatment can be energy neutral or even energy positive



Carbon and Energy Balance of Wastewater Treatment



Carbon Balance

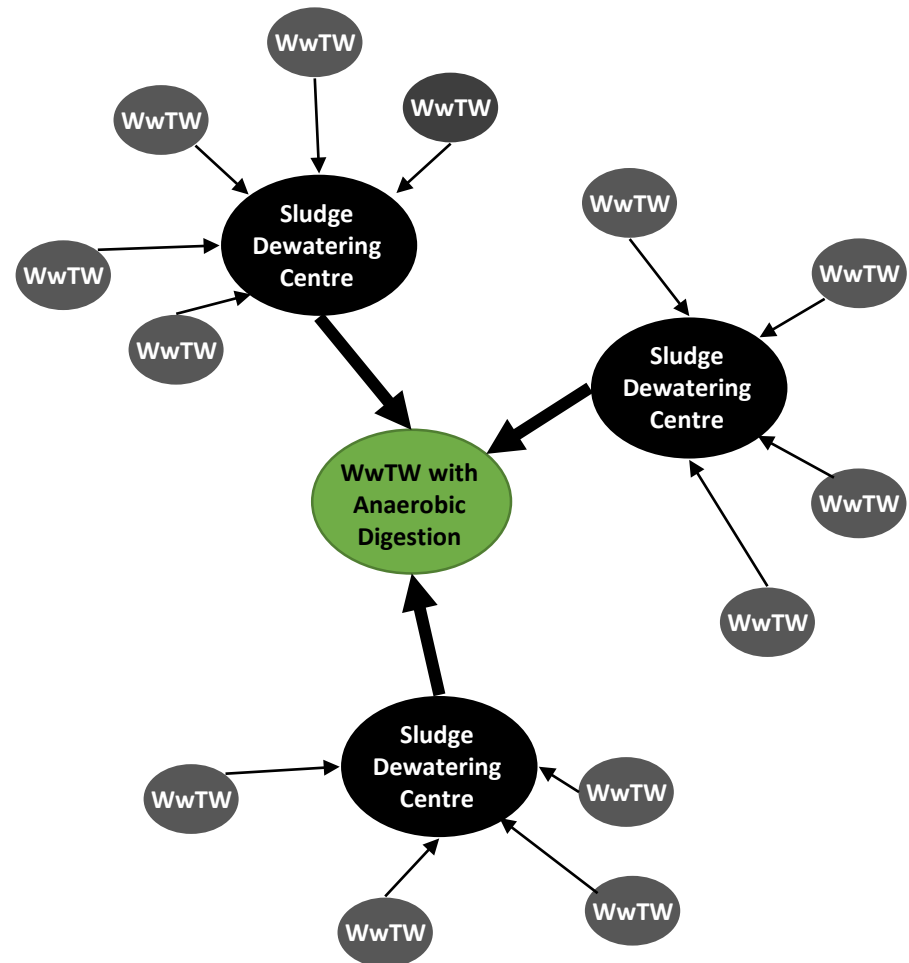
- 18% is recovered as CH₄
- 60% of C is loss
 - 6-12% in Final Effluent
 - 27-36% in CO₂ in Aeration
 - 30% in the Digested Sludge

Energy Balance

- 30% of Chemical Energy is recovered
- Excluding Pumping, Dewatering, the electrical energy consumption is equivalent to 3-4% of the inflowing energy
- If the produced chemical energy is converted into electrical energy, the NET electrical energy production (6-7 kWh) is equivalent to 6-7% of the inflowing chemical energy

Achieve Energy Neutral/Positive

- Not every wastewater treatment work has Anaerobic Digestion
- Transportation of the sludge **requires energy**
- Besides, Pumping, Screening, Sludge Dewatering, etc. **require energy**
- For achieving energy neutral/energy positive:
 - **Produce more energy**
 - **Reduce treatment related energy consumption**



Producing More Energy

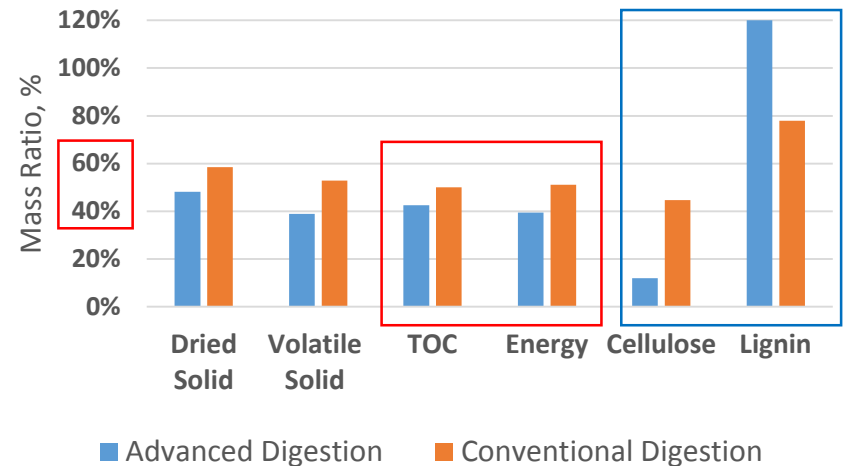
Improve Primary Settlement

- Increase AD feed
 - Improve Primary Settlement for capturing more COD/TOC and preventing **loss in Secondary Treatment**



With conventional coagulant
COD Removal: 40% → 70%
pCOD Removal: 50% → 90%

Unutilized Valuable Substance



Recovery from Digested Sludge

- Further recover energy from digested sludge (15 KJ/g)
 - Hydrolysing leftover **cellulose** and feed back to Digester
 - Pyrolysis, Gasification, Hydro-carbonization

Reducing Energy Consumption in Secondary

Advantages:

- Robust treatment performance
- Capable of removing Nutrient

Disadvantages:

- **Energy intensive (Aeration)**
- Oxidize part of TOC (~30%)

Current Approaches

Activated Sludge and Trickling Filter

- $\text{TOC} + \text{Energy} = \text{CO}_2 + \text{Biomass}$



Possible Alternative Technology

Microbial Fuel/Electrolysis Cell

- MEC: $\text{TOC} + \text{Energy} = \text{CO}_2 + \text{H}_2$
- MFC: $\text{TOC} = \text{CO}_2 + \text{Electricity}$

OR

Anaerobic Treatment

- $\text{TOC} = \text{CO}_2 + \text{CH}_4$

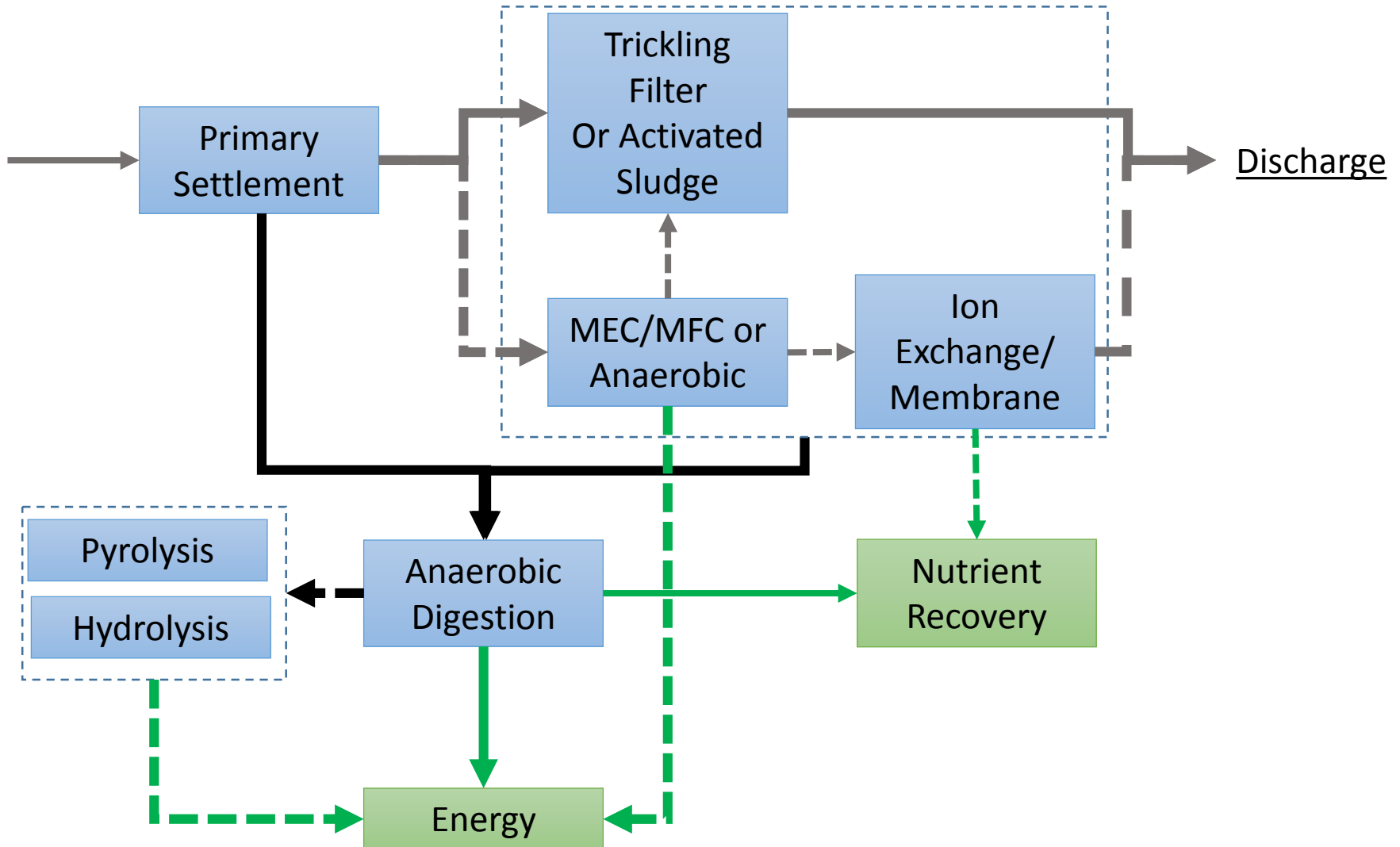
Advantages:

- Generate energy in the treatment process
- Less sludge production
- Less energy consumption

Disadvantages:

- **Incapable** of removing Nutrient
- Nutrient has to be removed by further biological or chemical treatment

Future Wastewater Treatment



Conclusion

- Supernatant of sludge dewatering process, which may contains about **12-30% of inflowing N** and **15-50% inflowing P**, is a good place to recover nutrient
- Recovering nutrient directly from wastewater can prevent considerable amount of nutrient lost in the wastewater treatment process.
- Wastewater treatment can be **energy neutral/positive**.
- For achieving energy neutral/positive, it is better to
 - *Improve Primary Settlement for **capturing** more COD/TOC and for **preventing** carbon/energy loss in Secondary Treatment*
 - ***Further recover** energy from sludge*
 - ***Reduce** energy consumption of secondary treatment, or even **generate** energy in the secondary treatment*

Thanks